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(a) Calculate the heat flux through the insulated sheet. Here, is the temperature difference, is the length of the insulated sheet along the direction of heat flow, and  $k$  is the thermal conductivity. Substitute for, 0.02 m for  $L$ , and for  $k$ .

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This is consistent with the fact that the surface heat flux in the positive  $y$  -direction is given by the following equation: From the sketch, the temperature gradient is positive. Therefore, the heat flux is negative. The heat transfer is in the negative  $y$  -direction, the plate is being heated by the fluid.

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ASSUMPTIONS: (1) Steady-state conditions, (2) Negligible heat transfer from the wire by natural convection or radiation.

ANALYSIS: If all of the electric energy is transferred by convection to the air, the following equality must be satisfied.

$P_{elec} = I^2 R = I^2 \rho L / A = h A_s (T_s - T_\infty)$  where  $A_s = \pi D L = \pi (0.0005 \text{ m}) (0.02 \text{ m}) \times 3.14 \times 10^2 = 52 \text{ m}^2$ . Hence,  $I = \sqrt{P_{elec} A_s / (h \rho L)}$

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FIND: (a) The heat flux through a 2 ... PROBLEM 1.1 KNOWN: Thermal conductivity, thickness and temperature difference across a sheet of rigid extruded insulation. Slideshare uses cookies to improve functionality and performance, and to provide you with relevant advertising.

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$dT/dx = -q''/k$ , is a constant, and hence the temperature distribution is linear. The heat flux must be constant under one-dimensional, steady-state conditions; and  $k$  is approximately constant if it depends only weakly on temperature. The heat flux and heat rate when the outside wall temperature is  $T_2 = -15^\circ\text{C}$

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Assumptions 1 Steady operating conditions exist. 2 Convection heat transfer coefficient is uniform. 3 Heat transfer by radiation is negligible. 4 Heat losses from the boiler are negligible.

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